Synthesis of magnetite and her used by AgNO₃ remove from aqueous system

Síntesis de magnetita y su uso en la remoción de AgNO3 de sistemas acuosos

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Abstract

Today pollution is an important problem that must be addressed, in this sense adsorption processes are a methodology that is usually used to remove different pollutants such as anions, cations and organic compounds. There is a great diversity of adsorbents ranging from porous oxides, metallic networks and polymeric membranes; magnetite and its composites have been shown to be adsorbent materials for the removal of various contaminants. The present work shows the study of the removal of Ag(I) from aqueous systems with Fe₃O₄ synthesized from precipitation processes. The magnetite showed an adsorption capacity of 19.84 mgg-1 according to the Langmuir adsorption model, a KL of 0.143 Lmg⁻¹ the partition coefficient showed a favorable adsorption with values between 0.1-0.01 and an endothermic Gibbs free energy. of 4.8 KJmol⁻¹. The kinetics of adsorption is carried out using a second order system, observing a decrease in the magnitude of the rate constant (K2) with the initial concentration of Ag(I), which suggests that the adsorption process at concentrations elevated is limited by the intra-particle diffusion of the system.

Magnetite, Adsorption, AgNO₃

Resumen

Hoy en día la contaminación, es un problema importante que debe de atenderse, en ese sentido los procesos de adsorción son una metodología que usualmente se utiliza para remover diferentes contaminantes como aniones, cationes y compuestos orgánicos. Existe una gran diversidad de adsorbentes que van desde óxidos porosos, redes metálicas y membranas poliméricas; la magnetita y compósitos de esta, se han mostrado como materiales adsorbentes para la remoción de diversos contaminantes. El presente trabajo muestra el estudio de la remoción de Ag(I) de sistemas acuosos con Fe₃O₄ sintetizada a partir de procesos de precipitación. La magnetita mostró una capacidad de adsorción de 19.84 mgg⁻¹ de acuerdo con el modelo de adsorción de Langmuir, una KL de 0.143 Lmg-¹, el coeficiente de reparto mostró una adsorción favorable con valores entre 0.1-0.01 y una energía libre de Gibbs endotérmica de 4.8 KJmol⁻¹. La cinética de adsorción se lleva a cabo mediante un sistema de segundo orden, observándose una disminución de la magnitud de la constante de velocidad (K2) con la concentración inicial de la Ag(I), lo que sugiere que el proceso de adsorción a concentraciones elevadas es limitada por la difusión intraparticular del sistema.

Magnetita, Remoción, AgNO3

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Introduction

Adsorption processes have been shown to be a good alternative for the removal of various contaminants in aqueous systems (metals, drugs, dyes, pesticides and others). This process has great advantages such as its simplicity, since they basically consist of placing the adsorbent with the aqueous system to be treated, either in bulk or in column [1,2], in addition to a wide range of adsorbents, such as polymeric membranes, mesoporous silica, metal oxides, MOFs, among others.

In this sense, the use of magnetite in various processes of adsorption of contaminants in aqueous systems has been published, for example Uranium (VI), Chunhui Luo et al. reported that the metal removal capacity improves with the presence of metal-reducing bacteria, associating the removal of uranium to the formation of FeUO4 species [3], the use of this metal oxide and its composites for the removal of various contaminants such as organic matter, dyes and other heavy metals such as Ni, Pb, Cd and Cr among others, both in aqueous systems and in soil, have also been reported [4-9].

The present work shows the study of the removal of Ag(I) in aqueous systems with magnetite synthesized by precipitation and hydrothermal treatment, the adsorption of the metal is evaluated using the Langmuir adsorption model, the effect of pH on the adsorption of the metal and the kinetics of adsorption of the same.

Experimental Section

Synthesis and characterization of Fe3O4

The synthesis of magnetite was carried out by precipitation techniques according to equation 1, with a 2Fe3+:Fe2+ ratio [10,11]. In a 250 mL flask, 5.27 g of FeSO4 and 2.7 g of FeC13 were dissolved in 200 mL of water under constant stirring, then the pH was adjusted to 10-11 with NH4OH and the system was placed at reflux for 24 h. At the end of this time, the magnetite was recovered by filtration and dried at 75°C for 12 h [10,11].

 $2\text{FeCI}_3 + \text{FeSO}_4 + 8 \text{ NH}_4\text{OH} \longrightarrow \text{Fe}_3\text{O}_4 + (\text{NH}_4)_2\text{SO}_4 + 6 \text{ NH}_4\text{CI} + 4 \text{ H}_2\text{O}$ Reaction 1 The magnetite was characterized by powder XRD, which was carried out on a RIGAKU ULTIMA IV X-ray diffractometer.

Adsorption studies of Ag(I) from aqueous systems

The evaluation of silver(I) adsorption capacity was performed by determining the adsorption kinetics at 10 min intervals for 1 h with standard solutions of AgNO3 at different concentrations (100-500 ppm). 0.1 g of the material was placed with 10 mL of a solution at 57, 123, 192, 319 and 694 mgL-1 of Ag and the residual concentration of silver in the solution was determined at the aforementioned times by atomic absorption spectrometry.

The adsorption capacity of silver was determined by equation 1, where qt is the loading at time t, Co and Ct are the concentrations of silver in the initial solution and at time t in mgL-1, V the volume of sample used (L) and m the mass of material used in g.

$$q_t = \frac{(C_o - C_t) V}{m}$$
(1)

Effect of pH on Ag (I) Adsorption

The effect of pH on the adsorption capacity of magnetite was evaluated by determining the adsorption capacity of magnetite at pH 3, 4.5, 6 and 10. 0.1 g of the material was placed with 10 mL of Ag(I) solution at the pH under study for 20 minutes and the concentration of residual Ag in the solution was determined.

Results and discussion

Figure 1 shows the diffractogram of the synthesized magnetite, corroborating the obtaining of this phase. The planes are observed at $2\Box$ at 30.1, 35.4, 43.1, 54.5, 57.6, 62°, which correspond to the magnetite according to Mohammadi et al].



Graphic 1 XRD Synthesized magnetite

Adsorption studies of Ag(I) from aqueous systems

Figure 2 shows the adsorption isotherms of Ag(I) with the synthesized Fe₃O₄, observing an adsorption equilibrium after 20 minutes of contact. A removal of 80 to 95% was observed at moderate concentrations of 57 to 200 mgL⁻¹ Ag, decreasing to 28% at high concentrations of 700 mgL-1 Ag (Figure 3).



Graphic 2 Adsorption isotherms of Ag(I) with Fe₃O₄



Graphic 3 Adsorption capacity of Ag(I) with Fe₃O₄

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The fit of the experimental data to the Langmuir and Freundlich adsorption models showed a poor fit to the Freundlich model (Figure 4b), fitting the experimental data only to the Langmuir model (Equation 2, Figure 4a), where Ce and qe refer to the concentration and charge at equilibrium of the system, KL represents the Langmuir constant and Q0 the maximum charge for the formation of the monolayer. This model assumes that adsorbate-adsorbate interactions are weak (physisorption) and that there are no adsorbate-adsorbate interactions [13, 14].

$$\frac{C_e}{q_e} = \frac{1}{K_L Q_0} + \frac{C_e}{Q_0} \tag{2}$$

Figure shows the fit 4a, of the experimental data to the Langmuir model, showing a maximum loading capacity (Q0) of 19.84 mgg-1 of Ag(I) and a Langmuir constant (KL) of 0.143 Lmg⁻¹. The Gibbs free energy was determined from Equation 3, where R is the gas constant (8.314 JK⁻¹ mol⁻¹), T the absolute temperature and KL the Langmuir constant; an endothermic adsorption process was observed with a magnitude of 4.8 KJmol⁻¹. The partition coefficient (RL), was determined according to Equation 4, where KL is the Langmuir constant and C0 the initial concentration of sorbate (Ag(I)); the magnitude of RL, is a parameter that allows identifying if the adsorption process is favorable or not; when the system presents values of RL=1, the adsorption process is linear, while values of RL=0 imply an irreversible adsorption process and for values of 0<RL<1, the adsorption process is favorable. The adsorption system of Ag(I) on Fe₃O₄, showed RL magnitudes in the range of 0.1-0.01, suggesting a favorable adsorption process.

$$\Delta \boldsymbol{G} = -\boldsymbol{R}\boldsymbol{T}\boldsymbol{l}\boldsymbol{n}\boldsymbol{K}_{\boldsymbol{L}} \tag{3}$$

$$\mathbf{R}_L = \frac{1}{1 + K_L C_0} \tag{4}$$

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Figure 4 Fit of experimental data to the model of (a) Langmuir and (b) Freundlich.

The adsorption kinetics was adjusted to the pseudo-second order model (Equation 5 and 6), where qe and qt, are the charges at equilibrium and at time t and K2 the velocity constant of the system. The velocity constant of the system, values from 0.22 to 0.057 gmg-1min-1 were observed. The rate constant decreases as the initial Ag(I) concentration of the system increases (Figure 5), suggesting that at high concentrations the adsorption mechanism is limited by intraparticle diffusion [13, 14].

$$\frac{dq_t}{dt} = K_2 (q_e - q_t)^2 \tag{5}$$

$$\frac{t}{q_t} = \frac{1}{K_2 q_e^2} + \frac{t}{q_e} \tag{6}$$

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Figure 5 Dependence of K_2 on the initial Ag(I) concentratio

Effect of pH on the adsorption of Ag(I) from aqueous systems with Fe_3O_4

Figure 6 shows the effect of pH on the adsorption of $[Ag(H_2O)_2]$ + with magnetite, a decrease in the adsorption capacity of the material is observed as the pH of the system increases, with 78% removal at acidic pH (3) and decreasing as the pH increases in the system, with only 51% removal at pH 6.0. This decrease is due to the change of the magnetite surface charge at pH higher than 3.0, which disfavors the Fe-Ag interactions and the adsorption process, at basic pH (3.0).

At basic pH (10), the quantitative removal of silver from the system is observed, this is due to the precipitation of Ag (OH) (Kps=1.5X10-8), which favors the removal of the metal by precipitation and not adsorption processes.



Figure 6 Effect of pH on the adsorption process of Ag(I)

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Conclusions

The removal of Ag(I) in aqueous systems with Fe_3O_4 , is favorable at acidic pH <3, where the highest metal removal is observed at 78 %. The removal capacity of silver with magnetite is moderate, according to the Langmuir model, the maximum loading capacity for the formation of the monolayer on the surface is 19.84 mgg^{-1} , the KL is 0.143 Lmg⁻¹. The adsorption kinetics is carried out by a second pseudo-order model, the rate constant decreases with respect to the initial concentration of silver in the system, suggesting intra-particle diffusion governs that the adsorption process at high concentrations, while external diffusion is the main resistance at low concentrations.

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